We claim

1. A process for the preparation of carbamates of general formula $R_1NHCOOR_2$ where R_1 and R2 may be same or different which comprises reacting urea having the formula $R_1NHCONHR_1$, or $R_1NHCONHR'_1$ wherein R_1 and R'_1 are selected from alkyl, aryl, cycloalkyl, arylalkyl and alkylaryl, with an organic carbonate having the formula R_2OCOOR_2 or $R_2OCOOR'_2$ wherein R_2 and R'_2 may be same or different and are selected from alkyl, aryl, alkylaryl and arylalkyl, at a temperature in the range of 120° C to 200° C in the presence of a catalytic amount of a solid base catalyst under constant agitation and recovering the desired product by conventional separation methods.
2. A process as claimed I claim 1 wherein said reaction is carried out for a period of 3 to 12 hrs.
3. A process as claimed in claim 1, wherein said solid base catalyst is selected from the group consisting of metal oxides, metal salt, mixed oxide, carbon, mounted base, alkali ions exchanged Zeolites and clay mineral such as Mg-Al hydrotalcite having Mg/Al ratio 2:1 to 5:1.
4. A process as claimed in claim 3 wherein said metal oxide is selected from the group consisting of SiO_2«H_2O (silica gel), $A1_2C$>3, PbO, MgO, ZnO, ZrO_2, Na_2O and K_2O
5. A process as claimed in claim 3 wherein said metal salt is selected from the group consisting of Na_2CC>3, K^CCb, KHCOa, and $(NH_4)2C0_3$.
6. A process as claimed in claim 3 wherein said mixed oxide is selected from the group consisting of PbO-ZrO, PbZrO3,SiO_2-MgO, SiO_2-CaO, SiO_2-ZnO and PbO_2-ZrO.
7. .A process as claimed in claim 3 wherein said mounted base is selected from the group consisting of NaOH, KOH, K_2CC>3, alkalimetal and alkaline earth metal on silica gel, alumina, and MgO.
8. A process as claimed in claim 3 wherein said alkali ions exchanged Zeolites are selected from the group consisting of Na or K-ZSM-5 and/or alkali impregnated zeolites , NaOH or KOH impregnated H-ZSM-5.
9. A process as claimed in any preceding claim wherein said solid base catalyst is employed in an amount of from 0.01-10%.
10. A process as claimed in claim 9, wherein said solid base catalyst is employed in an amount of from 0.01-80%, preferably, 10-70 %.

11. A process as claimed in any preceding claim, wherein said organic carbonate is employed in an amount in the range of from 10 to 90%, preferably 30 to 90 %.

12. A process as claimed in any preceding claim, wherein the organic urea is selected from the group consisting of N,N' dimethyl urea, N,N'p-tolylene urea, N,N'-o-Cl diphenylene urea, N,N'-m-Cl diphenylene urea, N,N'p-Cl diphenylene urea, N,N"p-nitro diphenylene urea, N,N' dimethyl urea, N,N' dicyclohexyl urea and any mixture thereof.

13. A process as claimed in any preceding claim, wherein said organic carbonate used is selected from the group consisting of diphenyl carbonate, dimethyl carbonate, dibutyl carbonate and mixture thereof.

14. A process as claimed in any preceding claim, wherein said solid catalyst is recyclable several times for efficient production of carbamates from organic urea and carbonate.

15. A process as claimed in any preceding claim, wherein carbamate obtained are N-phenyl phenyl carbamate, N-4-methylphenyl phenyl carbamate, N-2-chlorophenyl phenyl carbamate, N-3-chlorophenyl phenyl carbamate, N-4-chlorophenyl phenyl carbamate, N-4-nitrophenyl phenyl carbamate, N-methyl butyl carbamate, N-phenyl methyl carbamate, N-methyl methyl carbamate and N-cylohexyl methyl carbamate.